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Colloid particle size-dependent dispersivity

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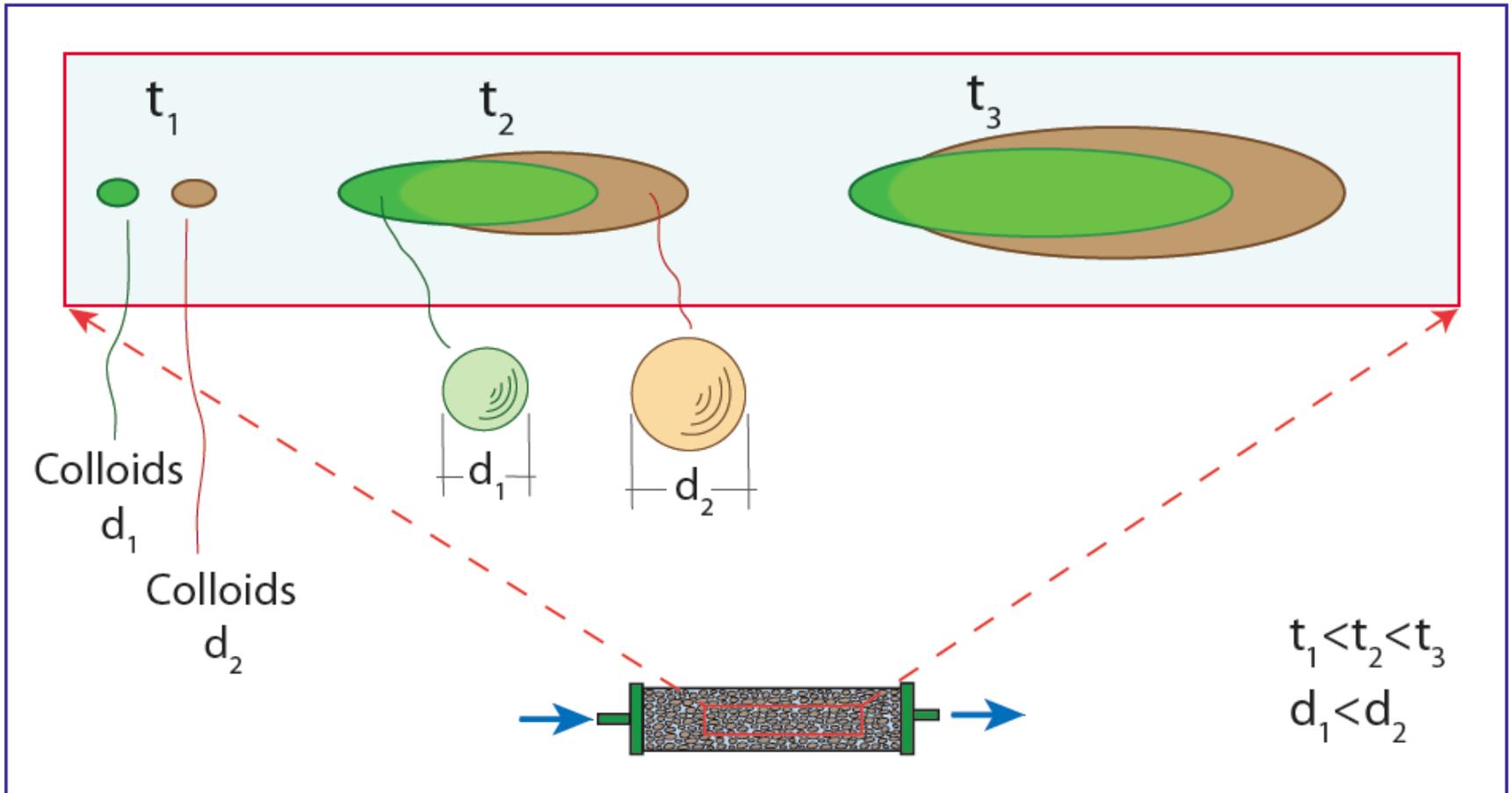
 **AGU FALL MEETING**

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H24E-02

 BioN Fate

Graphical abstract



Previous studies

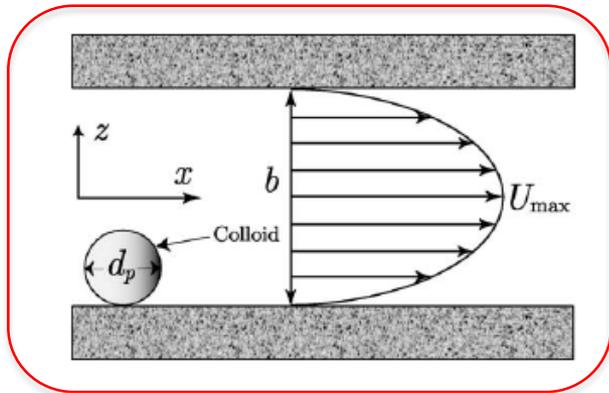
Early breakthrough of colloids as compared to conservative tracers

“Larger colloids are restricted by the size exclusion effect from sampling all paths”

References:

Toran and Palumbo, 1992
Powelson et al., 1993
Grindrod et al., 1996
Dong et al., 2002
Keller et al., 2004.
Vasiliadou and Chrysikopoulos, 2011
Sinton et al., 2012

Effective dispersion in a uniform fracture

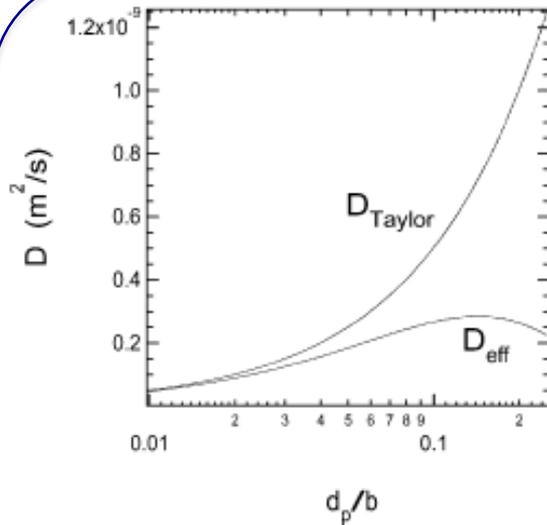


$$U_{\text{eff}} = \frac{2}{3} U_{\text{max}} \left[1 + \frac{d_p}{b} - \frac{1}{2} \left(\frac{d_p}{b} \right)^2 \right]$$

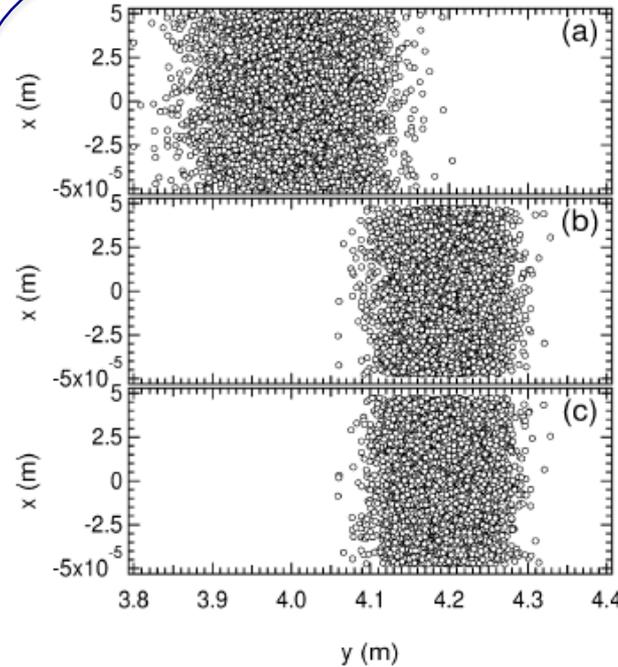
$$D_{\text{eff}} = D + \frac{2}{945} \frac{U_{\text{max}}^2 b^2}{D} \left(1 - \frac{d_p}{b} \right)^6$$

$$D_{\text{Taylor}} = D + \frac{2}{945} \frac{U_{\text{max}}^2 b^2}{D}$$

$$D = \frac{kT}{3\pi\eta d_p}$$



The effective particle velocity is increased, while the overall particle dispersion is reduced compared to Taylor dispersion, but with a tendency to increase with increasing particle size over a certain range of particle diameters.



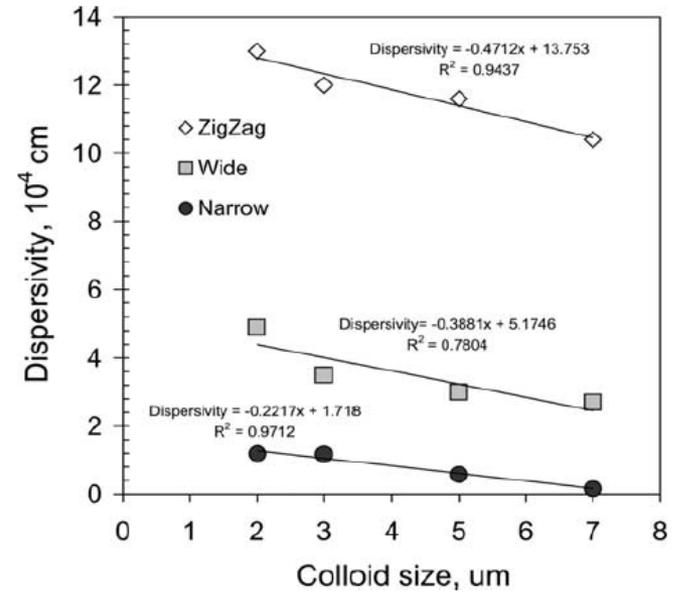
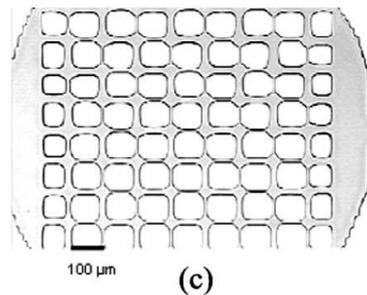
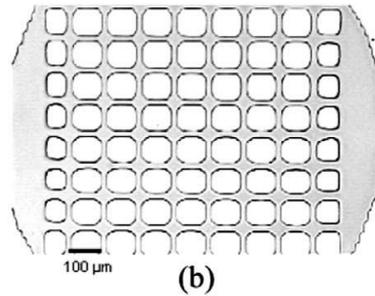
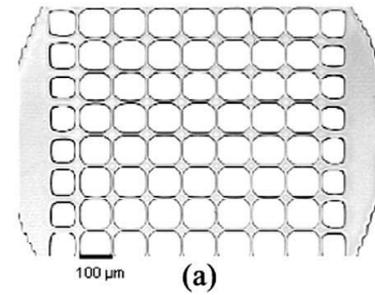
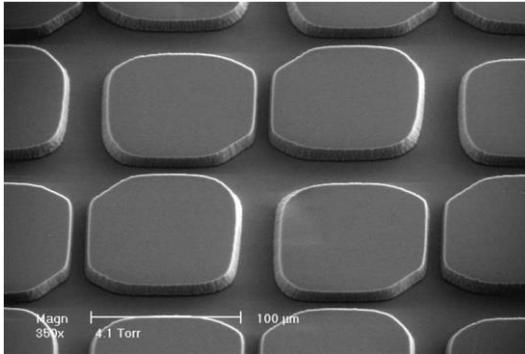
Infinitesimally small particles

2-D particle tracking (x,z)
 $d_p = 5 \times 10^{-6}$ m

1-D particle tracking (x)
with effective U & D
 $d_p = 5 \times 10^{-6}$ m

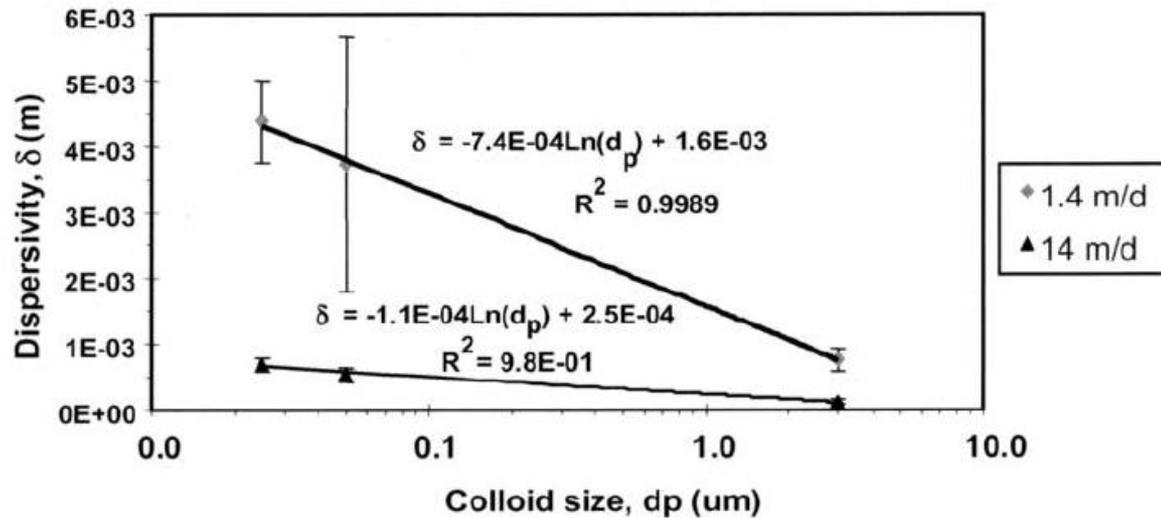
Snapshots of 5000-particle plume ($t=70$ d, $b=10^{-4}$ m)

Early work on particle size-dependent dispersivity (Micromodel)



Mass recovered: $M_r = 100\%$

Early work on particle size-dependent dispersivity (Column study)



Mass recovered: $M_r = 28.8$ to 41.0 %

Question: Should dispersivity decrease or increase with colloid particle size?

Another look
at
particle size-dependent dispersivity

Materials and methods

- Columns:** diameter = 2.5 cm
length = 15 & 30 cm
packed with glass beads ($d_c=2$ mm)
placed horizontally to minimize gravity effects
- Colloids:** fluorescent polystyrene microspheres
 $d_p= 28, 300, 600, 1000, 1750, 2100, 3000, 5000$ and 5500 nm
fluorescence spectrophotometry
- Tracer:** bromide in the form of NaBr (10^{-5} M)
ion chromatography
- Source:** “instantaneous” pulse
- d_p/d_c :** <0.00275
below the straining and wedging threshold of
>0.004 (Johnson et al., 2010) or
>0.003 (Bradford and Bettahar, 2006)

Transport experiments were performed under unfavorable colloid attachment conditions (pH=7, $I_s=0.1$ mM).

Mathematical Model

Governing transport equation

(Sim and Chrysikopoulos, 1998)

$$\frac{\partial C(t,x)}{\partial t} + \frac{\rho_b}{\theta} \frac{\partial C^*(t,x)}{\partial t} = D_L \frac{\partial^2 C(t,x)}{\partial x^2} - U \frac{\partial C(t,x)}{\partial x} - \lambda C(t,x) - \lambda^* \frac{\rho_b}{\theta} C^*(t,x)$$

Colloid attachment onto the solid matrix

$$\frac{\rho_b}{\theta} \frac{\partial C^*(t,x)}{\partial t} = k_c C(t,x) - k_r \frac{\rho_b}{\theta} C^*(t,x) - \lambda^* \frac{\rho_b}{\theta} C^*(t,x)$$

Assuming that $C^*(0,x)=0$

$$C^*(t,x) = \frac{k_c \theta}{\rho_b} \int_0^t C(\tau,x) \exp \left[- \left(k_r \frac{\theta}{\rho_b} + \lambda^* \right) (t - \tau) \right] d\tau$$

Initial and boundary conditions

$$C(0,x) = 0$$

$$-D_L \frac{\partial C(t,0)}{\partial x} + UC(t,0) = M_\delta \delta(t)$$

$$M_\delta = \frac{M_{in}}{A_c \theta}$$

$$\frac{\partial C(t,\infty)}{\partial x} = 0$$

Analytical solution

(Thomas and Chrysikopoulos, *JoCIS*, 2007)

$$\begin{aligned}
 C(t,x) = & \frac{M_\delta}{D^{1/2}} \exp\left[\frac{Ux}{2D_L} - Ht\right] \left\{ \frac{1}{(\pi t)^{1/2}} \exp\left[\frac{-x^2}{4D_L t} + \left(H - A - \frac{U^2}{4D_L}\right)t\right] \right. \\
 & \left. - \frac{U}{2D_L^{1/2}} \exp\left[\frac{Ux}{2D_L} + (H - A)t\right] \operatorname{erfc}\left[\frac{x}{2(D_L t)^{1/2}} + \frac{U}{2}\left(\frac{t}{D_L}\right)^{1/2}\right] \right. \\
 & + \int_0^t \frac{B\zeta}{\{B\zeta(t-\zeta)\}^{1/2}} I_1\left[2(B\zeta(t-\zeta))^{1/2}\right] \left\{ \frac{1}{(\pi\zeta)^{1/2}} \exp\left[\frac{-x^2}{4D_L\zeta} + \left(H - A - \frac{U^2}{4D_L}\right)\zeta\right] \right. \\
 & \left. \left. - \frac{U}{2D_L^{1/2}} \exp\left[\frac{Ux}{2D_L} + (H - A)\zeta\right] \operatorname{erfc}\left[\frac{x}{2(D_L\zeta)^{1/2}} + \frac{U}{2}\left(\frac{\zeta}{D_L}\right)^{1/2}\right] \right\} d\zeta \right\}
 \end{aligned}$$

$$A = k_c + \lambda, \quad B = \frac{k_c k_r \theta}{\rho_b}, \quad H = \frac{k_c \theta}{\rho_b} = \lambda^*$$

I_1 = Modified Bessel function (first-kind, order-one)

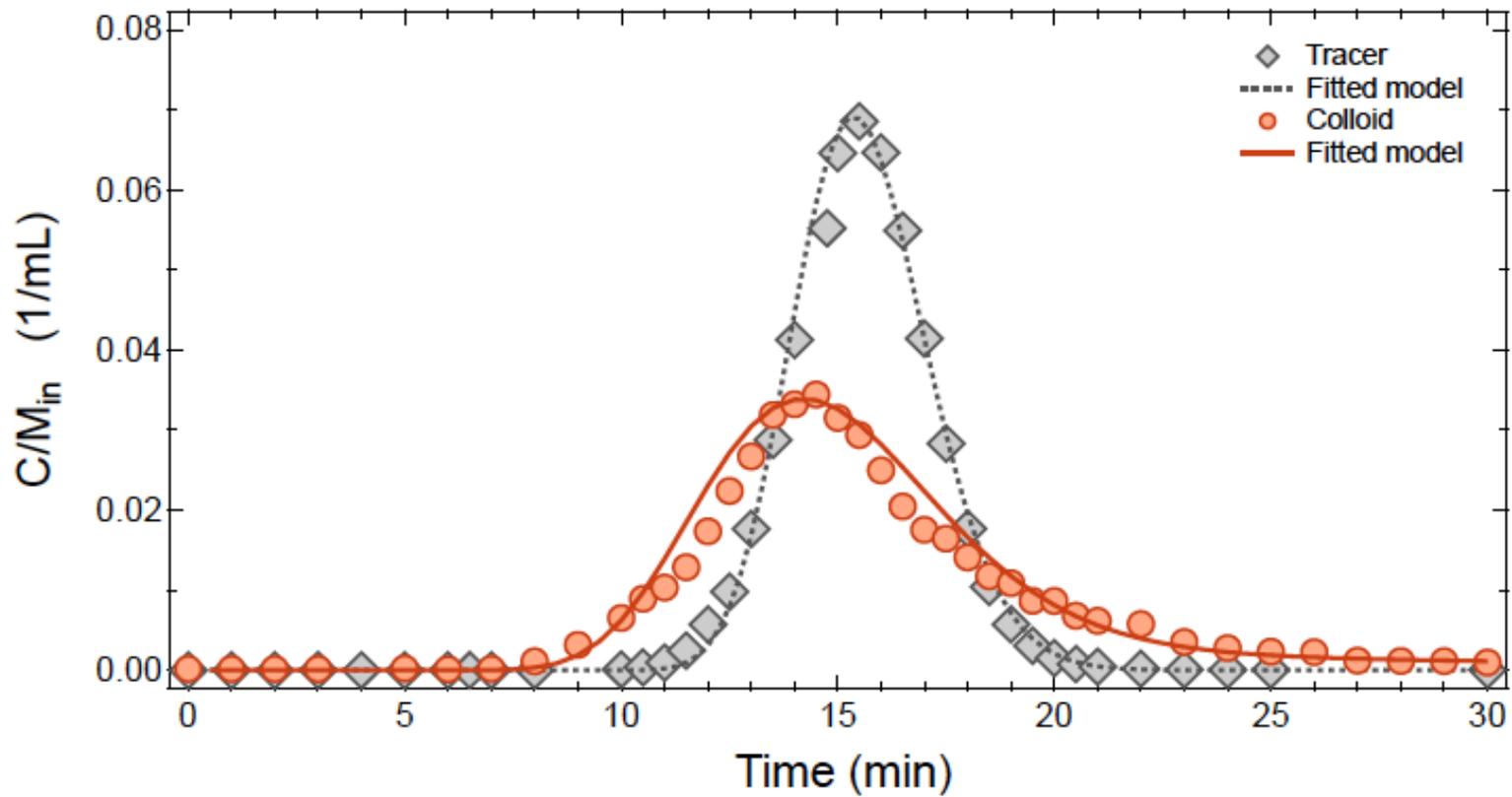


Figure 1. Early breakthrough

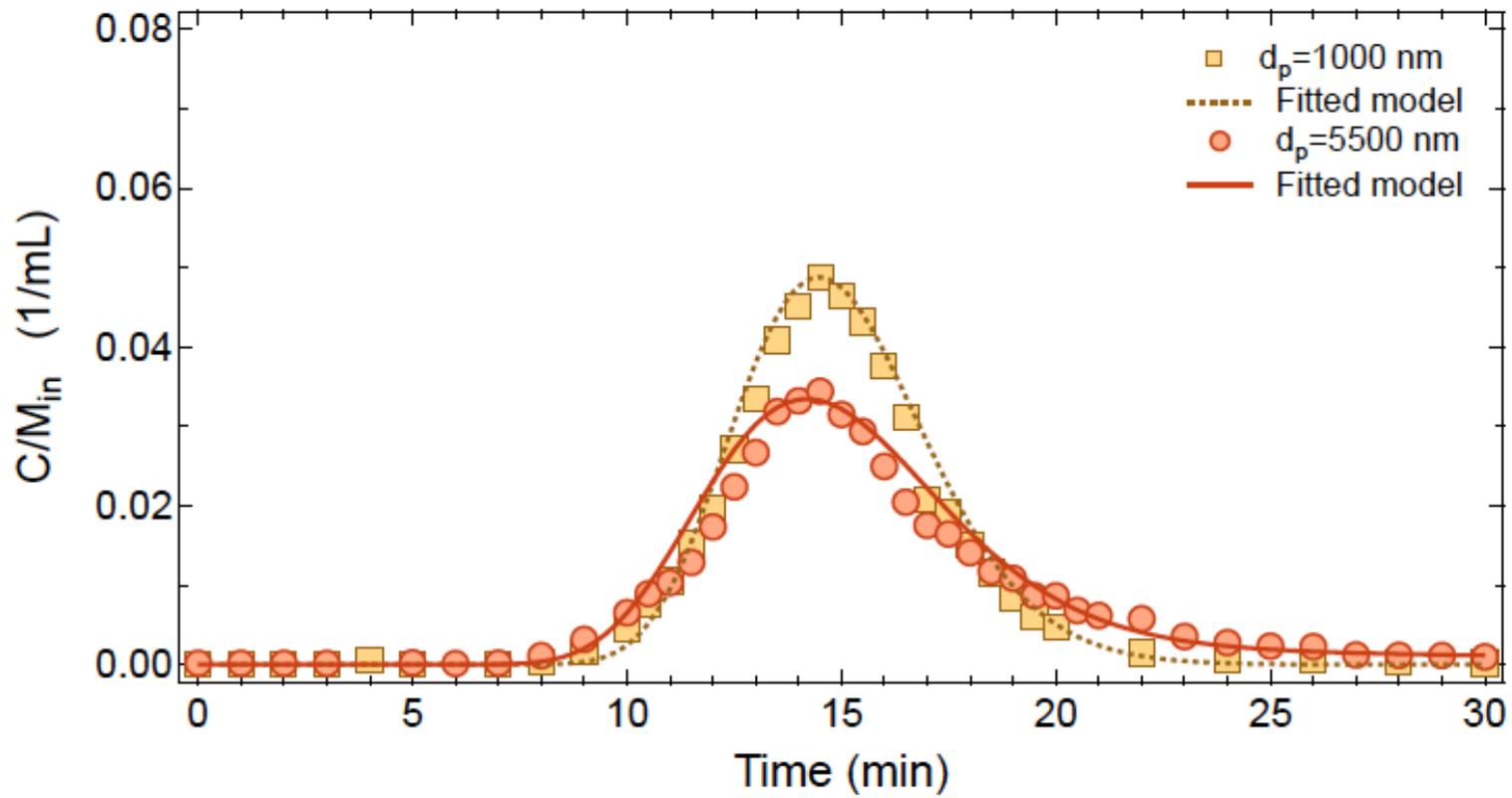


Figure 2. Breakthrough curves for two different colloids

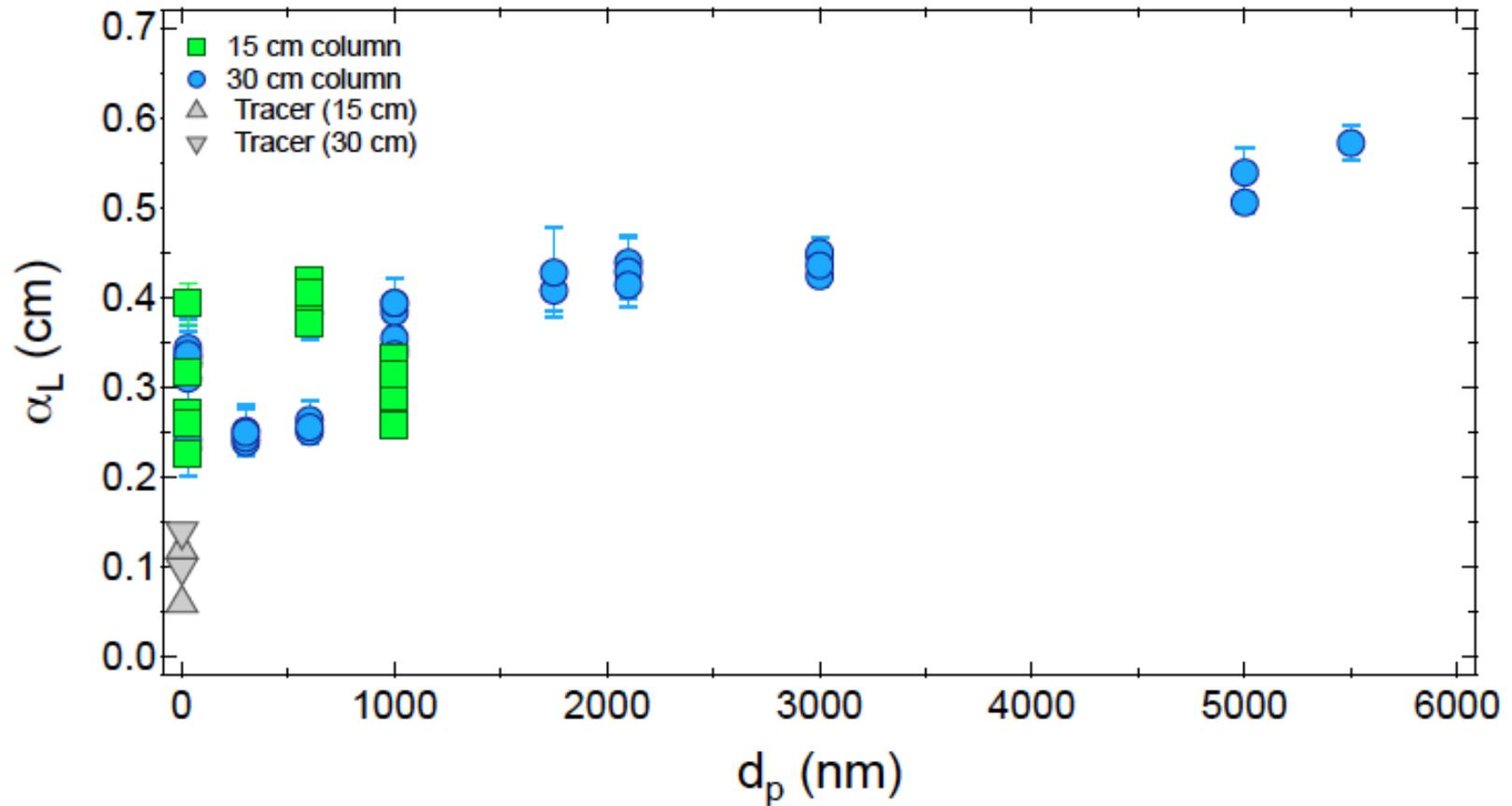


Figure 3. Longitudinal dispersivity as a function of colloid diameter.

Hypothesis that the population regression is linear: Accepted
 F test-Hypothesis that the slope=0: Rejected

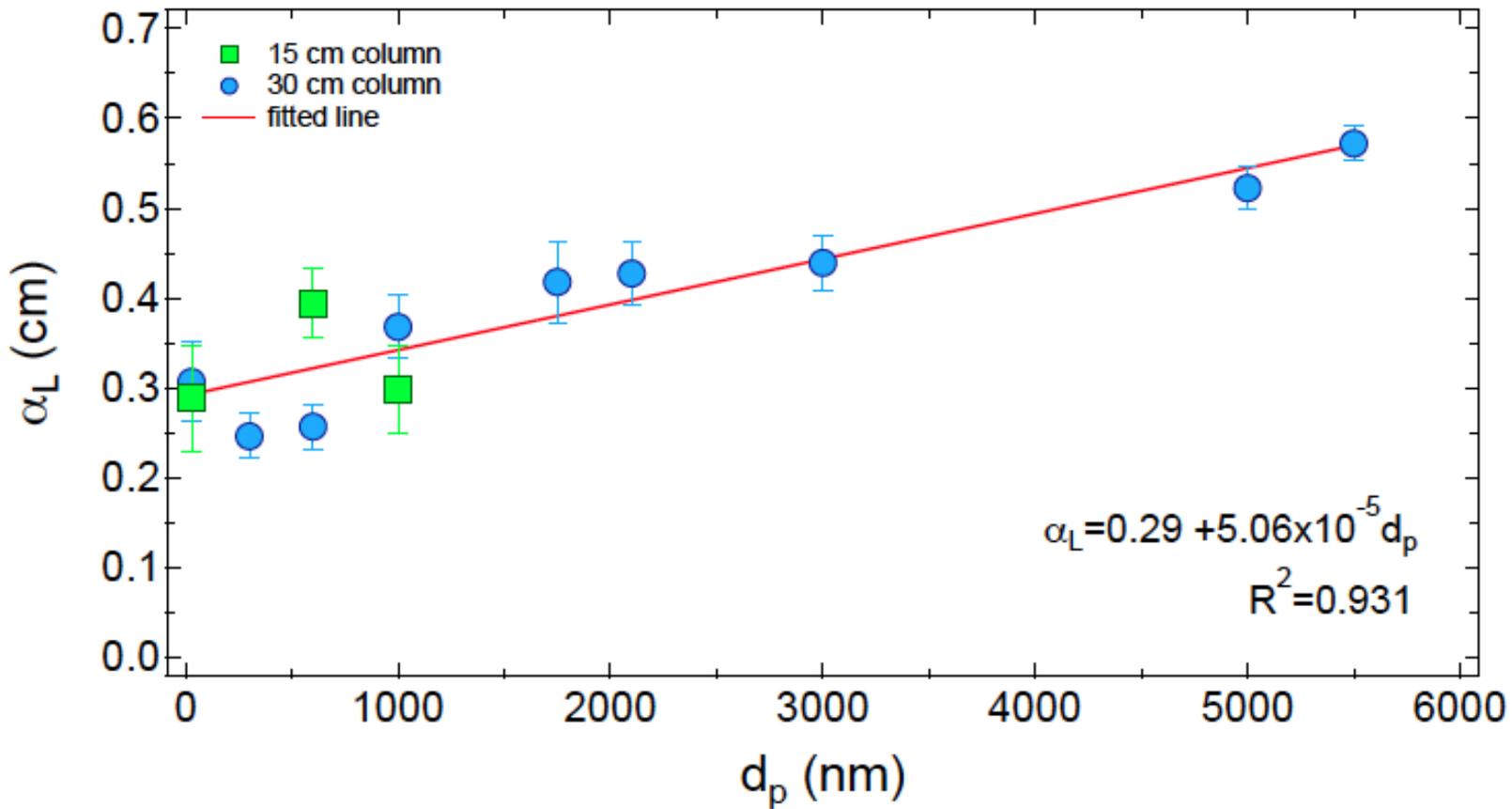


Figure 4. Longitudinal dispersivity (averaged) as a function of colloid diameter.

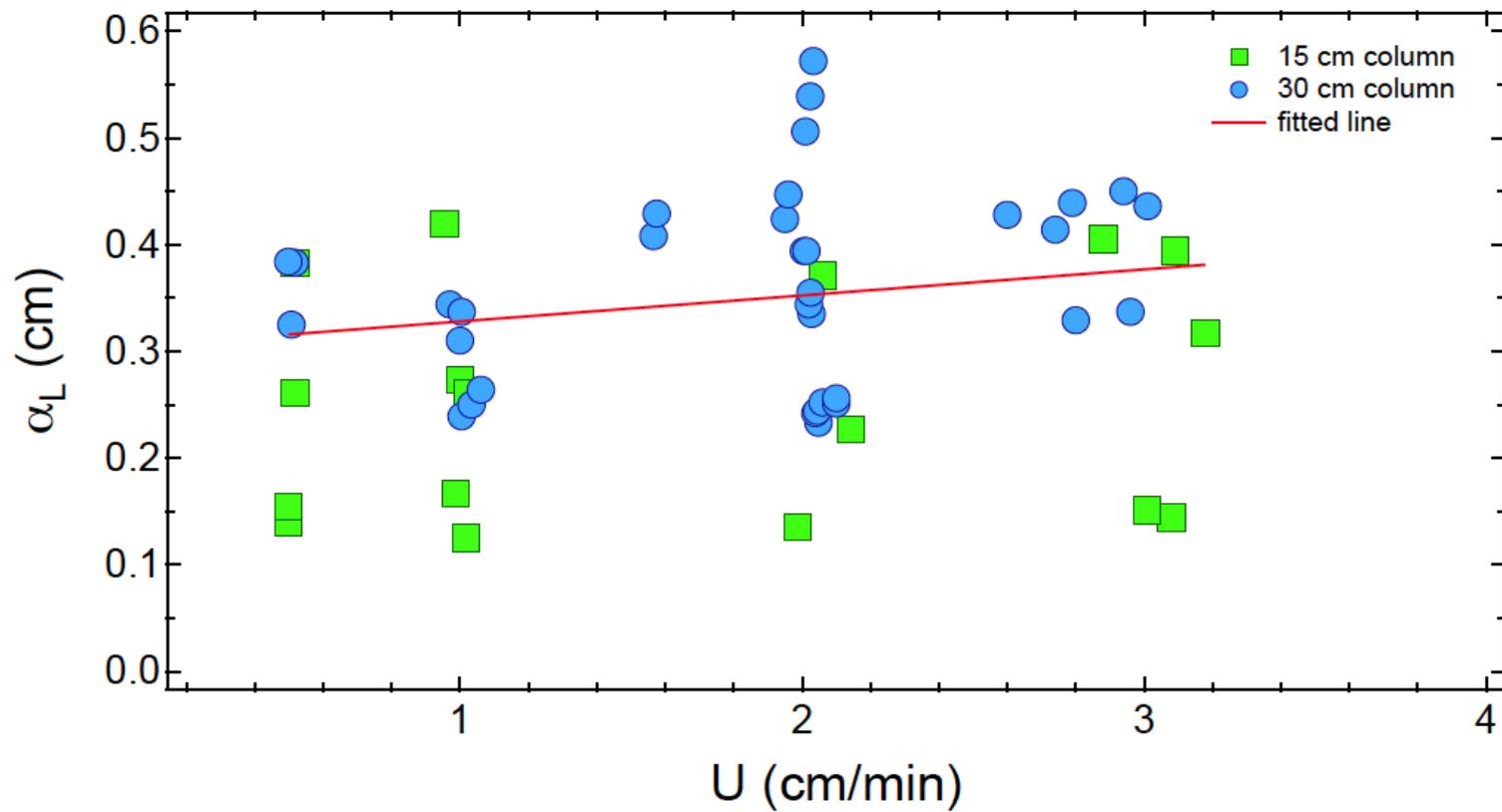


Figure 5. Longitudinal dispersivity as a function of interstitial velocity

Mass Recovery

$$M_r(L) = \frac{m_0(L)}{M_\delta / U}$$

$$m_0(L) = \int_0^\infty C(L,t) dt \quad \left[\frac{tM}{L^3} \right]$$

Zeroth absolute temporal moment

(Quantifies the total mass in the concentration distribution curve)

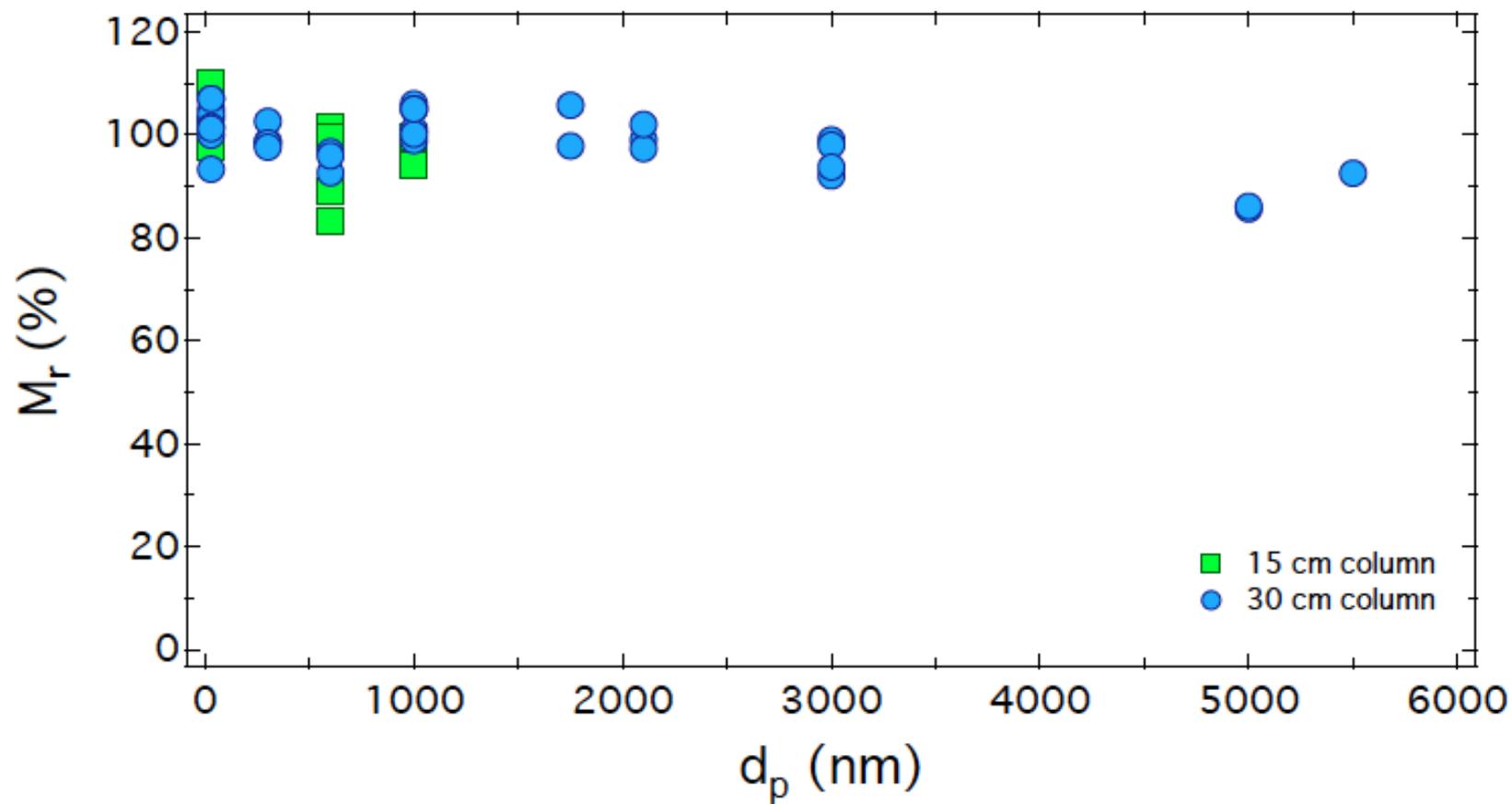


Figure 6. Mass recovery as a function of particle size

Scaling of D_L with Peclet number

(Delgado, 2007)

$$\frac{D_L}{\mathcal{D}_e} = \frac{Pe_m}{6} \left[\ln \left(\frac{3\tau}{2} Pe_m \right) - \frac{1}{4} \right], \quad Pe_m \gg 1$$

$$Pe_m = \frac{Ud_c}{\mathcal{D}_e} \quad [-]$$

$$250 < Pe_m < 10^5$$

Molecular diffusion is negligible.

Mechanical dispersion is the governing dispersion process.

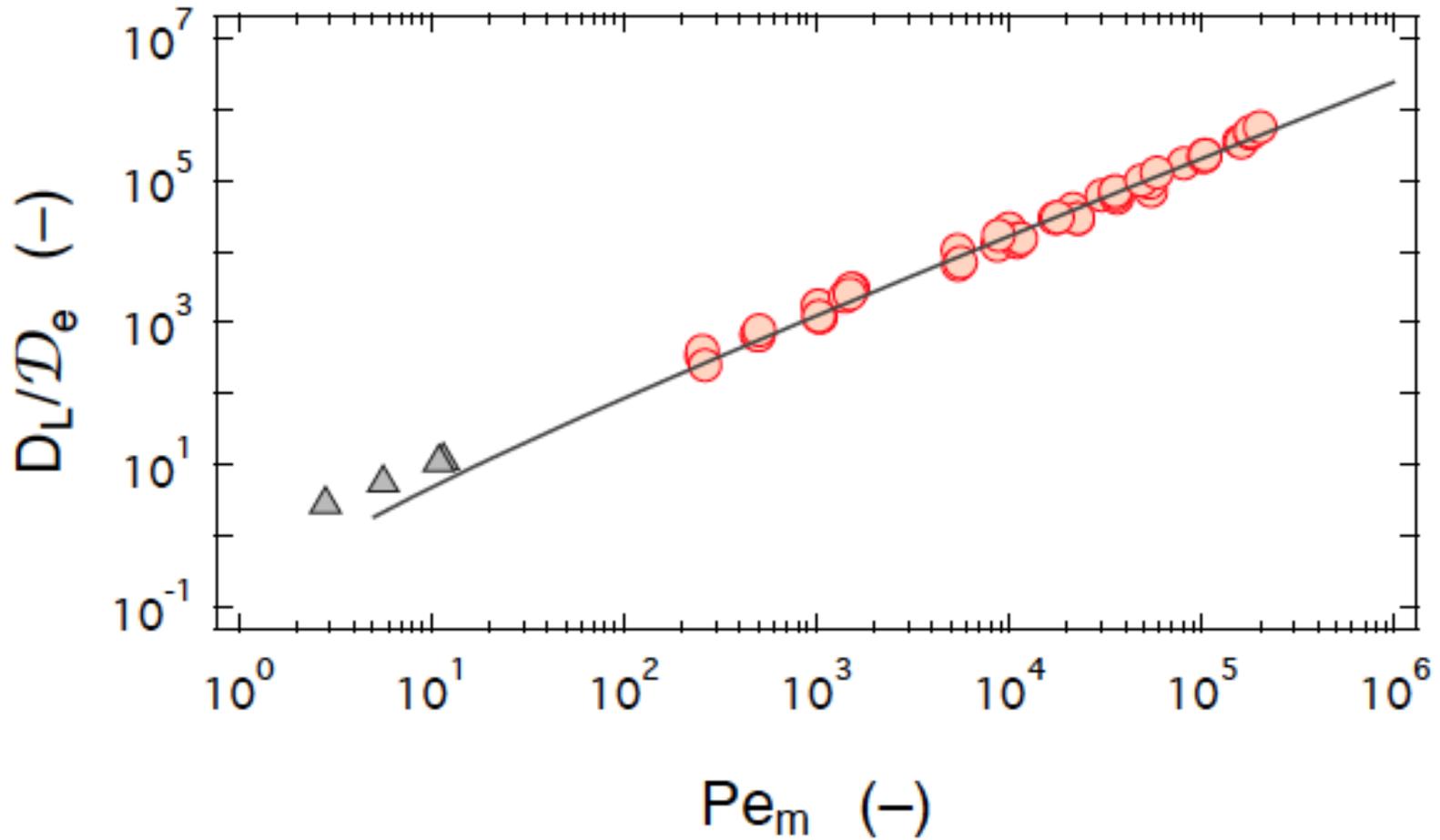


Figure 7. Scaling of the longitudinal hydrodynamic dispersion coefficients (circles for colloids, and triangles for tracer) with Péclet number.

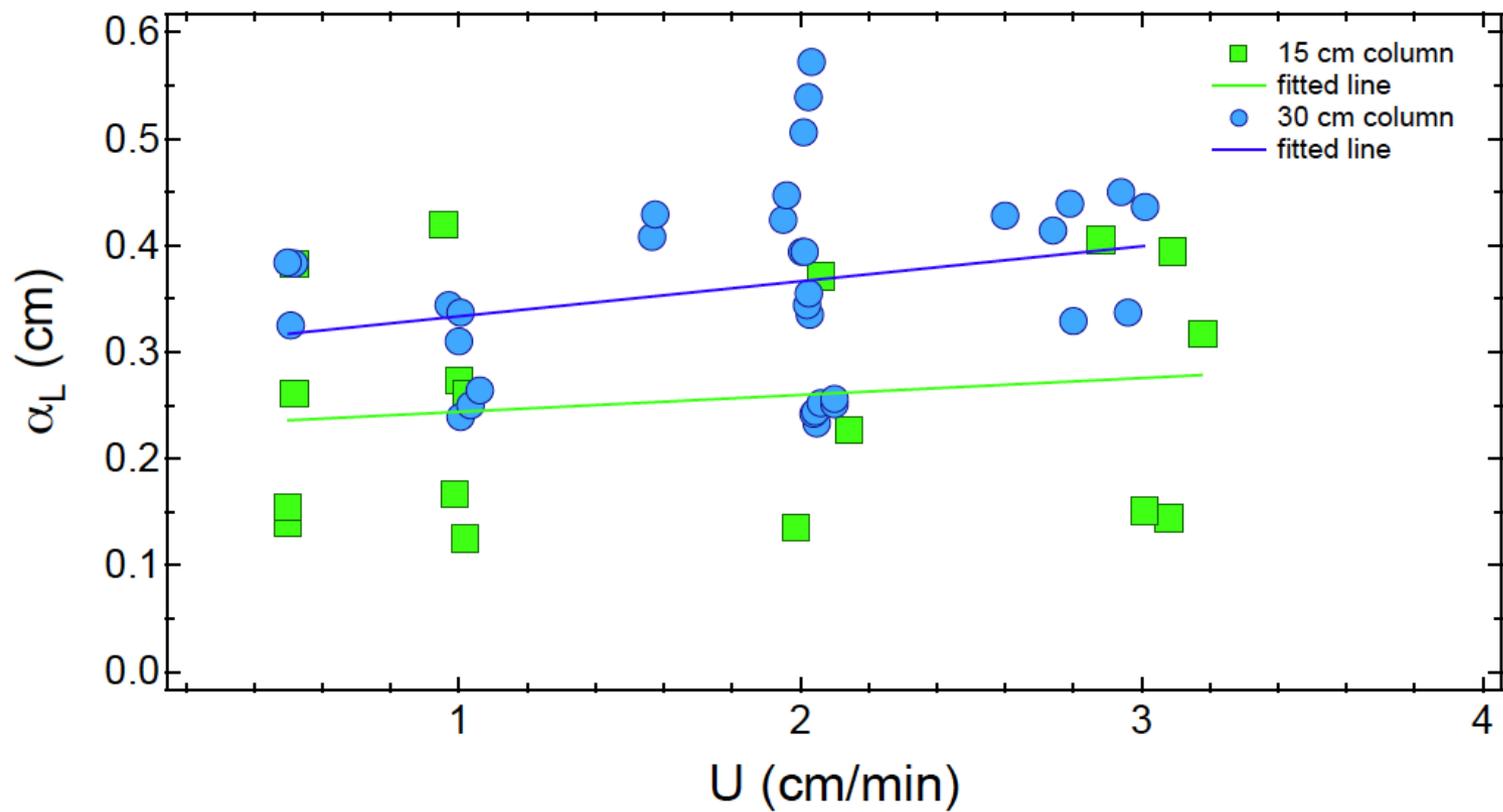


Figure 8. Longitudinal dispersivity as a function of interstitial velocity

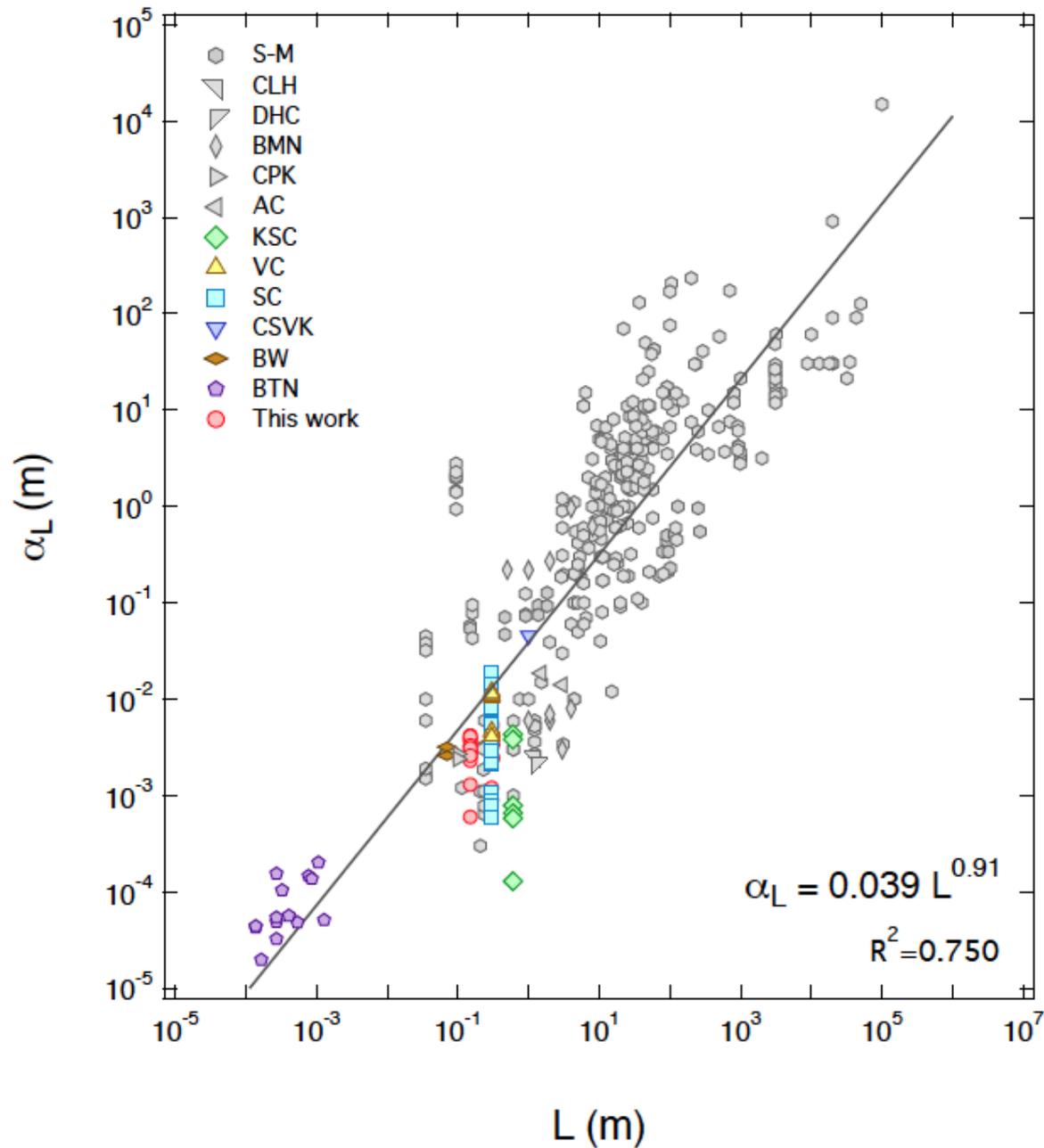


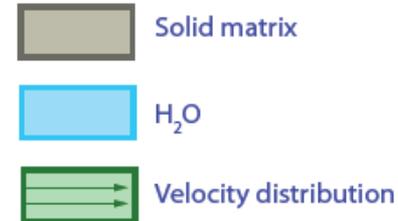
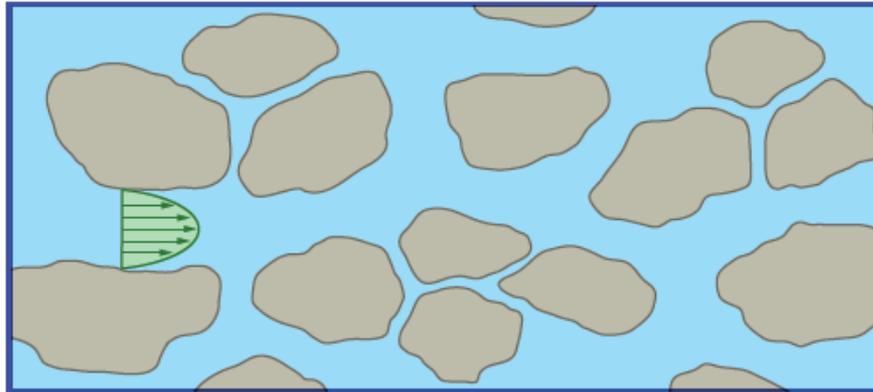
Figure 9. Compilation of 432 longitudinal dispersivities as a function of length scale. Molecular sized solutes are represented by gray symbols, and colloids/biocolloids by various colored symbols. The solid line is a standard linear regression line.

References:

- S-M [Schulze-Makuch, 2005]
- CLH [Chrysikopoulos et al., 2000]
- DHC [Dela Barre et al., 2002]
- BMN [Baumann et al., 2002]
- CPK [Chrysikopoulos et al., 2011]
- AC [Anders and Chrysikopoulos, 2005]
- KSC [Keller et al., 2004]
- VC [Vasiliadou & Chrysikopoulos, 2011]
- SC [Syngouna & Chrysikopoulos, 2011]
- CSVK [Chrysikopoulos et al., 2012]
- BW [Bauman and Werth, 2004]
- BTN [Baumann et al., 2010]

Explanation

(a) Tracer



(b) Colloids

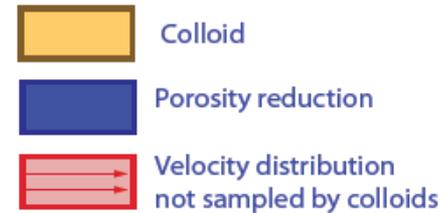
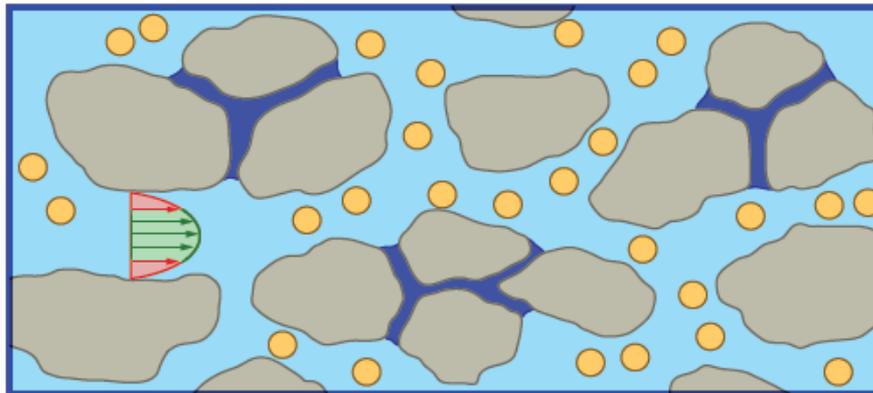


Figure 10. Schematic illustration of (a) solute and (b) colloid transport in water saturated porous media.

The tracer can sample the entire velocity spectrum within the parabolic profile (green region). Colloids do not sample the truncated portion of the parabolic velocity profile (red region). Also, colloids do not enter pore spaces with opening smaller than d_p , which essentially leads to reduction of effective porosity.

Summary

- Colloid dispersivity is not only a function of scale, but also a function of colloid diameter and interstitial velocity.
- Contrary to earlier results, colloid dispersivity increases with increasing colloid diameter and interstitial velocity.
- The observed increase in colloid dispersion is attributed to reduction of the effective porosity, which overbalances the reduction of colloid dispersion caused by colloid exclusion from the lower velocity regions.
- Fitted dispersion coefficients based on tracer data should not be used to analyze colloid data.
- The universal dispersivity line should be used with caution.

Thank you
for your attention